

Predicting the Particle Size Distribution in Twin Screw Granulation through Acoustic Emissions

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1 **ABSTRACT**

2 A non-destructive process analytical technology for monitoring the complex particle size
3 distributions inherent to twin-screw granulation (TSG) was presented, based on ultrasonic acoustic
4 emissions (AE). AE spectra were collected by discrete signal acquisition during the continuous
5 impacts of granules on an inclined plate positioned below the exit of an extruder. The paper
6 outlines the setup considerations associated with the impact plate, based on an examination of its
7 location, thickness (0.7, 1.0, 1.5 mm) and angle of inclination (10-60°) and the resulting particle
8 behavior at the plate, as determined by high-speed image analysis and AE monitoring.
9 Subsequently, AE spectra were collected during the wet granulation of lactose monohydrate at
10 different liquid-to-solid ratios from 8-14% and correlated with the particle size distributions (PSD)
11 to train a neural network model. Predicted PSD for particle sizes from 400 to 7000 μm based on
12 the AE spectra of validation trials showed the largest root mean squared error (RMSE) of 4.25
13 wt% at 2230 μm . After transforming the AE data with a newly created digital filter based on
14 particle impact mechanics to address auditory masking, the error for predicting fractions of each
15 particle size was significantly reduced to below 1 wt%. The technology shows great promise as a
16 monitoring method for TSG, being capable of predicting its complex size distributions in real time.

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20 mechanics, Artificial neural network

21 1. INTRODUCTION

22 The concept of continuous manufacturing has been gaining momentum in the pharmaceutical
23 industry over the past two decades. The publications of the United States Food and Drug
24 Administration (FDA) on process analytical technologies (PAT) along with the harmonized
25 tripartite Q8 guideline of the International Council for Harmonization (ICH) of ‘Technical
26 Requirements for Pharmaceuticals for Human Use’ paved the way for regulatory acceptance of
27 novel manufacturing technologies to be used in the production of solid oral dosage forms[1,2].
28 The advantages of continuous, in comparison to batch, manufacturing for drug products rely upon
29 its higher product consistency, reduced costs associated with product scale-up, and ability to
30 readily implement PAT[2,3].

31 Twin screw granulation (TSG) has gained much attention over the past decade as a continuous
32 manufacturing technology for wet, foam, heat-assisted and hot melt granulation[3–5]. The
33 advantages of TSG over other manufacturing technologies are its closely confined mixing
34 characteristics, short residence time (seconds compared to minutes or hours), and modular process
35 configuration, which dramatically reduce its equipment footprint[6,7]. One key difference between
36 TSG and its batch counterpart is the particle size distribution (PSD) produced. A batch granulation
37 process is expected to produce a unimodal (Gaussian) distribution whereas TSG typically produces
38 a bimodal distribution for the same formulation[6,8–10]. The PSD is vital to determining tablet
39 properties, such as strength and porosity, which ultimately affect the rate that this type of dosage
40 form disintegrates upon ingestion[11,12].

41 From a monitoring perspective, the challenges associated with a bimodal distribution are
42 unique, since simple numerical descriptors such as the mean particle size or the span of the
43 distribution have little correlated meaning with tableting, unlike for a Gaussian distribution. This

44 presents a unique need for PAT within TSG to show correlation with the PSD, not just simple
45 particle size descriptors, to monitor for quality consistency. PAT currently examined for in-line
46 granulation monitoring include near infrared (NIR) spectroscopy[13,14] and image
47 processing[11,14,15], though the latter is more prevalent industrially for particle sizing at the
48 moment. Both of these approaches have the advantage of being non-destructive and can be
49 integrated directly into the manufacturing process[13,14]. However, NIR spectroscopy requires a
50 large amount of data for calibration and it is subject to sensor fouling which can lead to spurious
51 results[16]. Image processing (ex. the commercial Horiba Eyecon™ system) is also subject to
52 fouling/dust accumulation around its optics and exhibits resolution issues when looking at
53 extremes in particle sizes[17,18]. Both are good non-destructive technologies with no risk of
54 interfering with or contaminating the granulation process but a more robust approach that was
55 immune to fouling would be advantageous if it could address the aforementioned complexities of
56 the PSD for TSG. Other potential techniques such as laser diffraction, mechanical vibrations, and
57 electrostatic sensing have been shown to be feasible to predict particle size but are difficult to
58 implement in a manufacturing setting due to their high costs, lower perceived sensor durability,
59 accuracy, and reliability [19–21].

60 Acoustic Emissions (AE) is an approach not yet considered for TSG monitoring but
61 conceivably well suited to the process based on its advantages of needing no calibrations, greater
62 immunity to the influences of fouling/dust accumulation, and low implementation costs[22]. It
63 would not be a completely novel approach since AE has been used for monitoring in the past of
64 other particulate process operations, both within[23–26] and outside[27–29] of the pharmaceutical
65 industry. The associated technique relate features of a detected signal to the particle impacts or
66 collisions that generated these acoustic emissions. Most notable examples have been reported for

67 high shear batch granulation, in order to determine the endpoint of the process and to predict a
68 Gaussian particle size distribution [26,30]. Outside the pharmaceutical industry, multiple studies
69 have involved pneumatic conveyers, fluidized beds, and milling units, using AE analysis to once
70 again predict a Gaussian distribution[19–22,29]. Approaches for applying AE to monitor much
71 more complex particle size distributions have yet to be disclosed in the literature.

72 In this regard, the present study investigates the means for developing a robust non-destructive
73 PAT capable of monitoring the complex PSD produced by continuous granulation via TSG. To
74 predict weight fractions for a broad range of anticipated granule sizes, it is postulated that the
75 intensity of a set of frequencies in an acquired AE spectrum can be correlated to the impact
76 mechanics of specific particle sizes. Furthermore, it is postulated that with appropriate signal
77 processing and selection of a neural network model that bimodal PSD may be predicted in real-
78 time for this continuous process.

79 **2. MATERIALS AND METHODS**

80 *2.1. Materials and Process Setup*

81 Granulation was completed in a 27 mm 40 L/D Model ZSE-27HP corotating twin screw
82 extruder (Leistritz Extrusion; Somerville, NJ, USA). The barrel consisted of a water-cooled feed
83 zone (Z0) and nine barrel zones (Z1–Z9) actively controlled at 35°C. The screw speed for all
84 experiments was 200 RPM. Flowlac® 100 α -lactose monohydrate (Meggler Pharma; Wasserburg,
85 Germany) was chosen as the placebo formulation for the study due to its low water solubility,
86 minimizing the effects of moisture on the acoustics during this preliminary stage of PAT
87 development. The lactose was introduced into the extruder at a constant flow rate of 4 kg/h for all
88 experiments using a Brabender T20 twin-screw gravimetric feeder (Mississauga, ON, Canada).
89 An aqueous solution of 4 wt% METHOCEL™ E3PLV (DuPont Nutrition & Biosciences;

90 Midland, MI, USA) was used as the liquid binder in this work and injected into the extruder at
91 zone Z2 using an ISCO 260D high pressure syringe pump (Teledyne-ISCO Inc.; Lincoln, NE,
92 USA) at varying liquid-to-solids (L/S) ratios of 8, 10, 12, 13, and 14%[31,32]. The liquid was
93 injected in the intermeshing region between the two screws. Experiments for each L/S ratio were
94 repeated 10 times to build a sizeable dataset for the modeling technique described in a later section.
95 The screw design employed for these experiments consisted of multiple conveying elements with
96 pitches of 30 and 20 mm from Z1-Z7 followed by two kneading blocks with discs at 60 degrees
97 offset in Z8 and then subsequent conveying elements in Z9; the screw design is typical for twin-
98 screw wet granulation.

99 *2.2. Particle Size Analysis*

100 The granules produced from the extruder were air-dried at room temperature for 48 hours to
101 below 5 % (w/w) moisture content before being analyzed for their size; moisture content was
102 determined using an HG63 moisture analyzer (Mettler-Toledo; Columbus, OH). PSD data was
103 determined using a Ro-Tap RX-29 sieve shaker (W.S. Tyler; Mentor, OH, USA). A granulated
104 sample of 100 g for each L/S ratio was originally classified into eight size fractions (using sieves
105 of 2100, 1700, 1400, 1180, 850, 500, and 300 μm nominal openings, as well as the bottom pan)
106 by mechanically agitating for five minutes. The weight difference before and after sieving was
107 used to find the wt% for each bin in the distribution. The mass on the 2100 μm sieve was
108 subsequently classified further by reconfiguring the shaker with sieves of 8000, 6300, 4760, 3350,
109 2360, 2100, and 1700 μm nominal openings and mechanically agitating for another five minutes.
110 Similarly, the mass in the bottom pan from the original agitation was subsequently classified
111 further by reconfiguring the shaker with sieves of 500, 300, 250, 180, 150, 53, and 44 μm nominal
112 opening and once more, mechanically agitating for five minutes. During the TSG experiments,

113 granule sizes changed from very fine to very coarse, much more broadly than normal granulation
114 operations. The sieving of the granules on the 2100 μm sieve and pan was done in order to capture
115 all possible changes across different L/S ratios for the neural network model implemented in the
116 subsequent section.

117 *2.3. Acoustic Signal Acquisition*

118 To record the continuous particle impacts exiting from the extruder, a F15 α broadband sensor
119 that was most sensitive to frequencies between 100 to 450 kHz (Physical Acoustics; Princeton, NJ,
120 USA) was attached to a 25.4 mm x 25.4 mm tab that extended from a SAE 304 stainless steel (SS)
121 impact plate with dimensions of 44.5 mm x 76.2 mm; seating the sensor on the tab, off to the side
122 of the plate, was preferred since the envisioned PAT design positions the plate inside the exit chute
123 of a TSG but ready access to the sensor will demand that it be positioned outside of the chute walls.
124 The sensor was fitted to the impact plate using high vacuum grease (Dow Corning) to improve
125 contact. Figure 1 shows the sensor and impact plate assembly.

126 The detected signal with the sensor was amplified using a Physical Acoustics 2/4/6c amplifier
127 set to +60 dB and collected using a National Instruments 3.5 MHz 12-bit 4-channel data acquisition
128 system. For each experiment, 30 seconds of data was collected from the collisions of granules onto
129 the plate at a sampling rate of 3 MHz. The vertical distance of the plate relative to the exit of the
130 extruder was based on an analysis of apparent terminal velocity to ensure consistency of the
131 impacts. Approximately 97% of the particles for Flowlac® 100 were below 250 μm [33] and so,
132 the smallest particle chosen to be a ‘granule’ in the model was 300 μm based on the minimum
133 sieve size in the study unlikely to capture ungranulated solids. The drop distance for a 300 μm
134 particle to reach terminal velocity was found to be roughly 20 cm below the exit of the extruder,
135 which is where the plate was positioned. This was done for all experiments mentioned below. The

136 terminal velocity analysis was done to ensure the impacts of particles at the top or bottom of the
137 plate would be relatively consistent with one another. Figure 2 shows a schematic for the
138 experimental setup with the extruder and impact plate assembly.

139 *2.4. Studies of Plate Angle and Plate Thickness*

140 Initially, the impact plate setup was examined for differing inclinations of 10, 30, 45, and 60
141 degrees relative to the horizontal plane with a fixed plate thickness of 0.7 mm. Only granulation
142 at 8% L/S ratio was tested in this case. AE sampling for a 30 s duration was repeated three times,
143 for every angle to account for statistical and acoustic variance. The trajectory and mechanical
144 integrity of granules colliding with the plate was observed at a distance of 10 mm away from the
145 edge of the plate by high speed image analysis taken using a FASTCAM SA-Z type 2100k camera
146 (Photron Limited, Tokyo, Japan) operating at 20,000 frames per second. Analysis of videos was
147 done using Photron FastCam Viewer 4 software.

148 In the second stage of experiments analyzing the impact plate setup, granule collisions were
149 recorded for 30 s for plates with thicknesses of 0.7, 1, and 1.5 mm at a fixed inclination of 60°. In
150 this case, more extensive granulation was performed at 8, 10, 12, 13, and 14% L/S ratios for each
151 plate thickness. The AE sampling for 30 s was repeated three times for every L/S ratio to account
152 for statistical and acoustic variance.

153 *2.5. Granulation Experiments for Model Training and Validation*

154 AE monitoring of particle collisions on the 1.5 mm thick impact plate angled at 60 degrees
155 inclination relative to the horizontal plane, were recorded according to Sec 2.3. TSG trials were
156 performed at L/S ratios of 8, 10, 12, 13, and 14%. At 8% it was found there was a large amount of
157 ungranulated particles whereas 14% was found to be the maximum saturation before the granules
158 turned into sludge. This range ensured AE spectra was collected from very fine to very coarse

159 granules. AE sampling for 30 s was repeated ten times per L/S ratio to generate a large training
160 dataset for modeling and to account for statistical and acoustic variance.

161 With an estimated flowrate of 1.1 g/s, a sampled signal of 30 s duration corresponded to
162 thousands or tens of thousands of collisions depending on the selected operating conditions with
163 the extruder. Factoring in repeats, more than 4,800 sampled signals were recorded for the training
164 and validation experiments. A discrete Haar wavelet filter was used to reduce noise followed by
165 Fast Fourier Transform (FFT) to view each processed signal in the frequency domain. With no
166 visible peaks roughly above 600 kHz, the chosen frequency range of analysis was 0-700 kHz in
167 this study. Each signal dataset was reduced in size for the model, decreasing the frequency
168 resolution from 3 Hz to 67 Hz.

169 A granular sample of roughly 300 g was collected for each L/S ratio after the 10 sampled
170 signals were collected. The PSD for the trial was determined by analyzing 100 g of the collected
171 granules. Three repeats were done to assess the error in the sieving measurement. Following the
172 characterization method in Sec 2.2, weight fractions were determined for the corresponding
173 average particle sizes (>8000, 7150, 5530, 4055, 2855, 2230, 1900, 1550, 1290, 1015, 675, 400,
174 275, 215, 165, 102, 49, and <44 μm). Weight fractions above 7150 μm and below 49 μm were
175 zero wt%, and did not change as the L/S ratio increased. As a result, the size fractions of >8000
176 and <44 μm were not included in the final dataset to reduce redundancies, making the final
177 distribution composed of 16 weight fractions in the model.

178 *2.6. Designing an AE Impact Filter*

179 A particle monitoring system based on impacts, where granules spanning a wide range of
180 sizes (and strengths) presents a challenge known as auditory or spectral masking. The “sound”
181 produced by a large particle impacting a plate will overshadow the sound produced by a smaller

182 particle colliding at the same time or closely thereafter. Since the principle of an acoustic
 183 monitoring method is to relate the amplitude of a signal (or specific frequencies in the signal) to a
 184 count of particles, masking may have a detrimental effect on the predicted PSD. To address this
 185 issue, a digital signal filter was conceived to alleviate auditory masking at the impact plate, derived
 186 from Hertz theory for single particle impacts.

187 The work by Rao describes the transverse response, normal modes, along with the force
 188 response when an impact force is applied to a metal plate at rest [34]. They are shown in Equations
 189 (1), (2), (6), and (7) below. The transverse response of the plate shown in Equation (1) below is a
 190 function of both the normal modes of the plate along with the plate response to the force applied.

$$w(x, y, t) = \sum_{m=1}^{\infty} \sum_{n=1}^{\infty} W_{mn}(x, y) \eta_{mn}(t) \quad (1)$$

191 where W_{mn} represents the normal modes of the plate and η_{mn} is the plate response to the force
 192 applied. m and n correspond to the modal numbers for the x and y direction. The normal modes
 193 are of the plate are:

$$W_{mn} = \frac{2}{\sqrt{\rho h a b}} \sin\left(\frac{m\pi x}{a}\right) \sin\left(\frac{n\pi y}{b}\right) \quad (2)$$

194 where ρ , h , a , b are the density, thickness, length, and width of the plate, respectively. Assuming
 195 the particles are spherical and collisions are elastic, the force can be modelled with the Hertz theory
 196 of impact as shown [35,36]:

$$F(t) = F_0 \sin\left(\frac{\pi t}{t_c}\right) = F_0 \sin(\pi \Omega t) \quad (3)$$

197 with F_0 being the maximum force and t_c being the contact time of a collision, and Ω is the
 198 frequency of the impact force. Expressions for the maximum force and contact time are given in
 199 Equations (4) and (5), respectively:

$$F_0 = 1.917\rho_1^{\frac{3}{5}}\left(\frac{1-v_1}{\pi E_1} + \frac{1-v_2}{\pi E_2}\right)^{-2/5} R^2 V_0^{6/5} \quad (4)$$

200

$$t_c = 4.53\left(\frac{4\rho_1\pi\left(\frac{1-v_1}{\pi E_1} + \frac{1-v_2}{\pi E_2}\right)}{3}\right)^{2/5} R V_0^{6/5} \quad (5)$$

201 where ρ_1 is the density of the particle, v_1 and E_1 refer to the Poisson ratio and Young's Modulus
 202 of lactose monohydrate. R is the particle radius and V_0 is its impact velocity. Knowing the impact
 203 force, the response of the plate to the force can be determined and is shown as:

$$\eta_{mn}(t) = \frac{2F_0}{(\omega_{mn}^2 - \Omega^2)\sqrt{\rho h a b}} \sin\left(\frac{m\pi x_0}{a}\right) \sin\left(\frac{n\pi y_0}{b}\right) (\omega_{mn} \sin \Omega t - \Omega \sin \omega_{mn} t) \quad (6)$$

204 where x_0 and y_0 are the points of impact on the plate, and ω_{mn} is the natural frequency of the
 205 plate:

$$\omega_{mn} = \pi^2 \left[\left(\frac{m}{a}\right)^2 + \left(\frac{n}{b}\right)^2 \right] \sqrt{\frac{E_2 h^3}{12(1-v_2)\rho h}} \quad (7)$$

206 where E_2 and v_2 are the Young's Modulus and the Poisson's ratio for the plate, respectively. The
 207 plate compression for a single particle dropping onto a plate was then computed from Equation
 208 (1). The parameters used in Equations (1) – (7) are shown in Table 1.

209 Figure 3 (a) shows the plate response, on a frequency basis, for the impact of a 100 μm
 210 particle. The plate response of a single granule of 49 to 7150 μm size impacting a stainless steel

211 plate at its epicenter, on a frequency basis, is shown in Figure 3 (b). As particle size increases, the
212 plate is seen to vibrate at a lower frequency, giving an inverse relationship. This trend was also
213 noted by others[37–39] and allows the user to understand and roughly correlate peaks in the
214 spectrum with their particle size.

215 Assuming granules impacting the plate are spherical in nature, the mass of a single granule
216 is calculated per particle size (49 – 7150 μm). It is assumed that the maximum mass of any particle
217 that will strike the plate is equal to the flowrate in g/s over a one second basis (1.1 g in this study).
218 The maximum mass is divided by the mass of every particle to obtain an approximate number of
219 granules per particle size. The theoretical amplitude for each particle size is then scaled by the
220 number of granules for its respective size. The measured amplitude from the AE experiments is
221 then divided by the maximum amplitude at the theoretical impact frequency found in Figure 3 (c)
222 to filter for auditory masking and produce the final spectrum.

223 2.7. Neural Network Model

224 To relate the data-intensive impact acoustic signal to particle sizes, an artificial neural network
225 (ANN) model was employed due to the exhibited nonlinearity in the modelled environment. These
226 types of models have been shown to be superior to statistical modeling when looking at highly
227 non-linear systems[40–42], making them attractive for the purposes of predicting PSD from an AE
228 signal. Before modeling, stratified splitting was used to ensure the training and testing sets
229 contained an equal proportion of data for each L/S ratio. Each L/S ratio dataset was split into 80%
230 training and 20% testing. Then 10% of the training data was used for validation during model
231 training. Principal component analysis (PCA) was used on the training set to reduce the dataset
232 dimensions down to 12 components which contain 64.5% of the variance in the original data. Both
233 PCA and the ANN were setup in Python using the *sklearn* library.

234 For the case of the testing set, the acoustic signal from granule collisions for each L/S ratio
235 were averaged in the testing set giving one representative spectrum for each L/S ratio. This strategy
236 allows for simplicity when performing new experiments as well as gives the opportunity to see the
237 prediction error for each distribution. When predicting PSD with the testing set, loadings from a
238 PCA model were used to convert the dataset into scores. The scores are then fed into the ANN to
239 predict the PSD. The ANN employed an input layer with 12 nodes, which correspond to the
240 number of components from PCA. This was followed by 3 hidden layers at 500 nodes, 250, and
241 100 nodes, respectively along with one output layer with 16 nodes, corresponding to each particle
242 size. The Rectified Linear Unit activation function (ReLU) was used for the input and first hidden
243 layer. The second and third hidden layers had the hyperbolic tangent (tanh) and sigmoid function,
244 respectively, while the output layer had a linear activation function. 50% dropout regularization
245 was employed between layers to minimize overfitting. The chosen Loss function was the mean
246 squared error (MSE). To quantify prediction error in the model, the root mean squared error
247 (RMSE) was used.

248 For the case when the model used the AE Impact Filter, the training, testing, and validation
249 datasets were identical to the original approach. In this case, PCA was not used to compress the
250 AE data since it was found to worsen predictions when the filter was used. The ANN architecture
251 was identical to the case without the filter, both in terms of the activation functions and number of
252 layers. The only difference being the input layer had 10395 nodes due to PCA not being used to
253 reduce the dataset.

254

255

256 **3. RESULTS AND DISCUSSION**

257 *3.1. Effect of Impact Plate Angle*

258 Exiting granules from the extruder were targeted to collide at the epicenter of the plate to
259 optimally minimize both plate vibrations and AE signal attenuation. The incline angle of the
260 impact plate will have a strong influence on the amplitude of acoustic emissions due to the contact
261 mechanics present. Figure 4 plots the average maximum amplitude in the spectra collected for
262 inclined plate angles of 10, 30, 45, and 60 degrees relative to the horizontal plane. The maximum
263 amplitude was seen to increase as the incline angle increased until 45 degrees, reflecting the gain
264 in AE signal intensity associated with particle impacts. This seems contrary to expectation, at least
265 following the theory of single particle impacts which anticipates the amplitude of AE associated
266 with a collision should be greater for smaller inclinations [39]. The trend seen for amplitude was
267 attributed to the accumulated mass observed on the plate over time at angles of 10 and 30 degrees,
268 dampening the impact force of subsequent colliding particles. Conditions at 45 and 60 degrees
269 showed no accumulated mass on the plate but as expected, the amplitude decreased for the steeper
270 angle in these two cases due to decreasing normal collision forces by falling particles.

271 Based on the trend in maximum amplitude, it might be naturally assumed that the choice
272 for plate inclination in the setup would have been at 45 degrees; however, the effects of granular
273 breakage and secondary collisions on the spectra must also be considered. Figure 5 shows the
274 captured motion of granules colliding with the impact plate at 45 and 60 degrees inclination, as
275 observed by high speed image analysis. At 45 degrees, more granular damage was observed during
276 the primary collision with the plate and rebounding particles had a greater chance of striking the
277 plate again. At 60 degrees, the decreased normal force reduced the damage seen by granules as
278 they collided with the plate and since they departed the field of view by ‘sliding or rolling’, there

279 was little likelihood of a detectable secondary impact. Despite the lower signal amplitude at 60
280 degrees, this condition was chosen as the preferred plate incline angle.

281 It is expected that some granule breakage will always occur regardless of the inclination
282 angle of the plate. Such breakage has more influence on a rebounding rather than an impacting
283 particle and hence, more significantly affect the PSD rather than acoustic emission in our study.
284 Fortunately, the absence of detectable breakage in the captured video of impacts at 60 degrees
285 inclination gave increased confidence that the signal was being correlated to an accurate
286 representation of the particles that produced the acoustic emissions.

287 *3.2. Effect of Impact Plate Thickness*

288 The other setup parameter studied was plate thickness. Figure 6 shows AE spectra for plates
289 of different thicknesses, constantly inclined at 60 degrees to the horizontal plane. There was
290 generally no change in the nature of the spectra for the same L/S ratio as the thickness increased
291 from 0.7 to 1.5mm; however, the signal amplitude decreased as the thickness of the plate increased,
292 most notably seen for the spectra at 13 and 14% L/S ratios. Particle impacts onto the 0.7 mm plate
293 were creating detectable vibrations in the plate itself during experiments implying particles might
294 contact onto the plate multiple times during a single collision event due to the rebound motion of
295 the plate, thereby increasing the measured amplitude. As its thickness increased the plate vibrated
296 less from the particle impacts. A thickness of 1.5 mm was considered acceptable for the final setup
297 since no motion from the plate was observed during experiments, and yet the signal strength was
298 sufficient for the model to distinguish different particle collisions.

299 *3.3. Signal Analysis based on Particle Size*

300 Figure 7 shows the average acoustic spectra from the TSG experiments for each L/S ratio
301 along with their respective PSDs. The observable trend in AE spectra, shown in Figure 7(a), was

302 a decrease in the amplitude as L/S ratio increased, with the main regions of interest being 50-150
303 kHz and 200-300 kHz. From plate response calculations in Figure 3(b), the 50-150 kHz region
304 corresponds to 300 – 1000 μm particle impacts and the 200-300 kHz region relates to 150 – 240
305 μm particle impacts. Correspondingly, Figure 7(b) shows that as the L/S ratio increased, the weight
306 fraction of granules between 49 – 1550 μm decreased substantially, seeming to corroborate the
307 decrease in amplitude in the AE spectra. While the plate response frequency assignments were
308 derived only for single particle impacts, they appear to be suitably correlated with the particle sizes
309 under this study from TSG. Impacts of particles above 2200 μm in size were predicted to produce
310 plate responses around 20-50 kHz, beyond the ideal sensitivity range of the broadband sensor. AE
311 associated with these larger particles still exhibited detected frequencies (harmonics) in the
312 experiments that could be discriminated by the model but the current setup should be considered
313 reasonable for monitoring particles below 3000 μm . Since the largest granule size suitable for
314 tableting is 1.25 mm[43–45], the current setup was considered suitable for the purposes of
315 introducing the ANN model. Future studies will consider the advantages of a two sensor system
316 to acquire a broader range of frequencies so that the model might have a better capacity to predict
317 very coarse granules via TSG.

318 *3.4. Model Training and Validation*

319 Confidence in the model predictions was evaluated based on RMSE calculated for the
320 testing AE spectra corresponding to granulation at each L/S ratio, as shown in Figure 8. Predicted
321 PSDs based on the testing datasets processed without and with the impact filter are shown in Figure
322 9 and 10, respectively along with their experimentally measured PSD for each L/S ratio. For the
323 case of processing the AE data without the impact filter, the RMSE for the majority of particle
324 sizes was below 2 wt% for all L/S ratios. This is reflected in Figure 9 where the model was able to

325 fit each PSD fairly well. The particle size with the highest error was 2230 μm for PSD at 12% L/S
326 ratio, which goes up to 4.25 wt% RMSE as seen in Figure 8 (a). This high RMSE is attributed to
327 the PSD being strongly bimodal with both peaks being nearly equal to one another, which likely
328 increased the difficulty in predictions. In general, the model without the filter was considered to
329 have satisfactorily learned to associate the AE spectra to sets of particles colliding with the impact
330 plate, at least for the specific case of lactose monohydrate which granulates at much lower degrees
331 of saturation than most pharmaceutical formulations. Future studies will be required to understand
332 how formulations and degree of saturation affect the AE spectra and the model's ability to
333 associate acoustics to particle size. This will enable the prediction error for each particle size to be
334 tracked for different formulations making this potentially a very powerful monitoring tool when
335 producing multiple products from the same TSG.

336 For the case of processing the AE spectral data with the impact filter, a significant
337 decrease was seen in the prediction error in comparison to Figure 8(a), now at or below 1 wt%
338 RMSE for all particle sizes being considered. This improved accuracy in predicted PSD is reflected
339 in Figure 10 where the model and experimental sieved weight fractions are much closer in value.
340 With the impact filter, the loss error was no longer localized around 2230 μm , highlighting the
341 effect that auditory masking was having on the AE signal in the original model. Diminishing
342 auditory masking of the signal allowed the model to more equally consider the contribution of all
343 frequencies (and particle collisions) in the response.

344 **4. CONCLUSION**

345 Ultrasonic acoustic emissions were explored as an approach for PAT to monitor the exiting
346 particle size from a twin screw granulator, a continuous granulation method noted for producing
347 complex size distributions. The elements of the approach consisted of a 1.5 mm thick stainless

348 steel impact plate, ideally inclined at 60 degrees to minimize powder accumulation and ensure
349 rebounding trajectories did not allow for secondary collisions by granules from the granulator.
350 Using an artificial neural network model and PCA to reduce the dimensions of the dataset, error
351 analysis showed the model experienced the most difficulty predicting the distribution when it was
352 strongly bimodal, with the highest reported error of 4.25 wt% for the 2230 μm fraction. Applying
353 a newly introduced impact filter to the AE data to minimize auditory masking, the model error
354 decreased significantly below 1 wt% and became evenly distributed amongst all particle sizes
355 rather than being localized to the larger particles in the exiting distribution. For this preliminary
356 study for an AE-based PAT approach, the training was done with lactose monohydrate, but future
357 studies will follow to examine how formulation and level of saturation affects acoustic emissions
358 of impacting granules. It is anticipated that plate design and the auditory masking filter will require
359 revisions as fracture strength and cohesiveness change the nature of particle impacts. Practically
360 speaking, the accuracy of the approach will also need study as the flow rate increases to production
361 levels and only a fraction of the exiting mass is impacting the plate.

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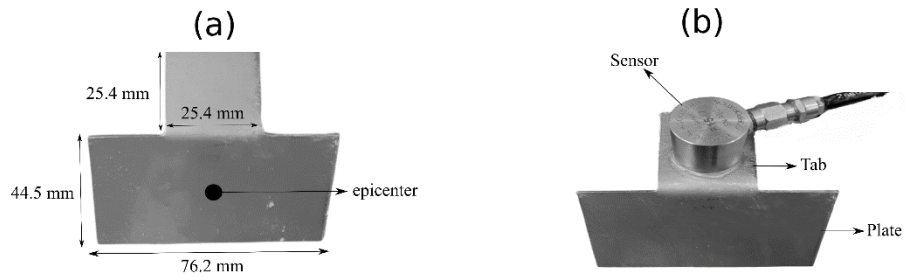
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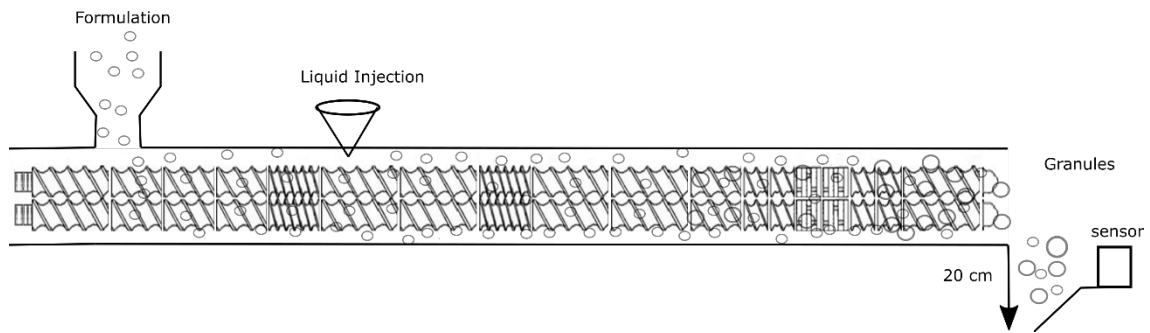
513 FIGURES



514

515 Figure 1. Top-down view of the impact plate inclined at 60 degrees relative to the horizontal plane

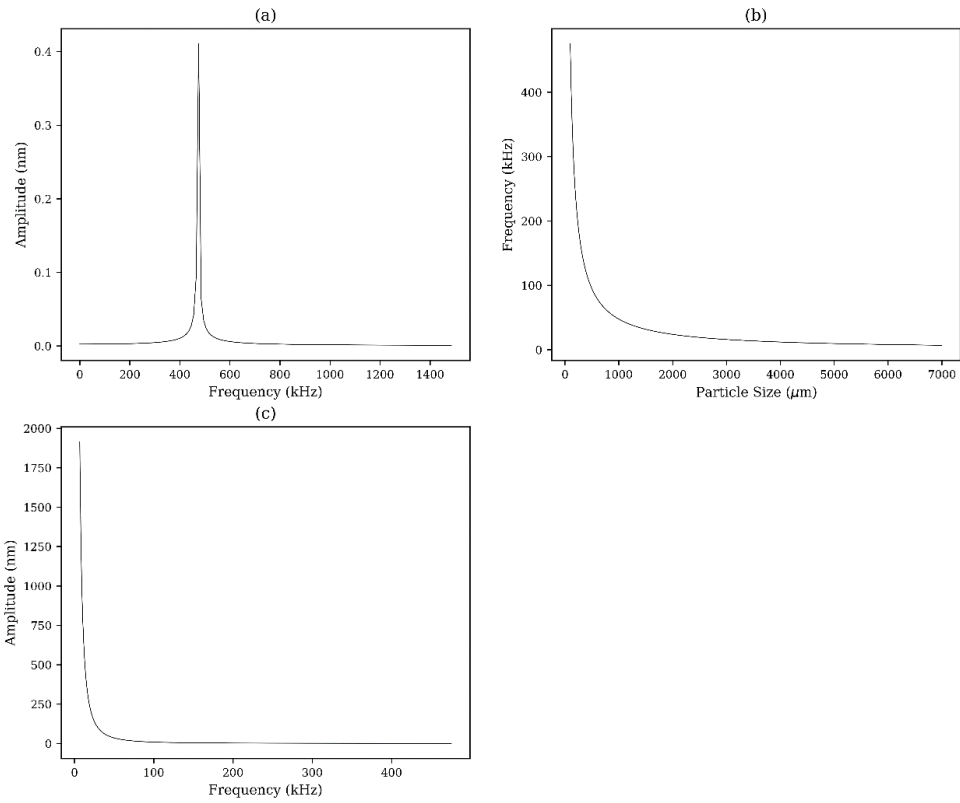
516 (a) without and (b) with the acoustic emission sensor.



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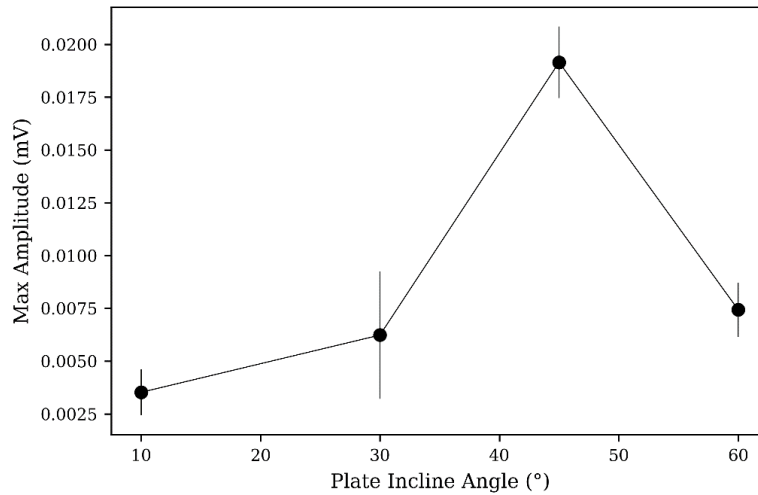
518 Figure 2. Schematic of the PAT setup for particle size monitoring, showing the twin-screw

519 granulator and impact plate assembly positioned after its exit in the experiments.



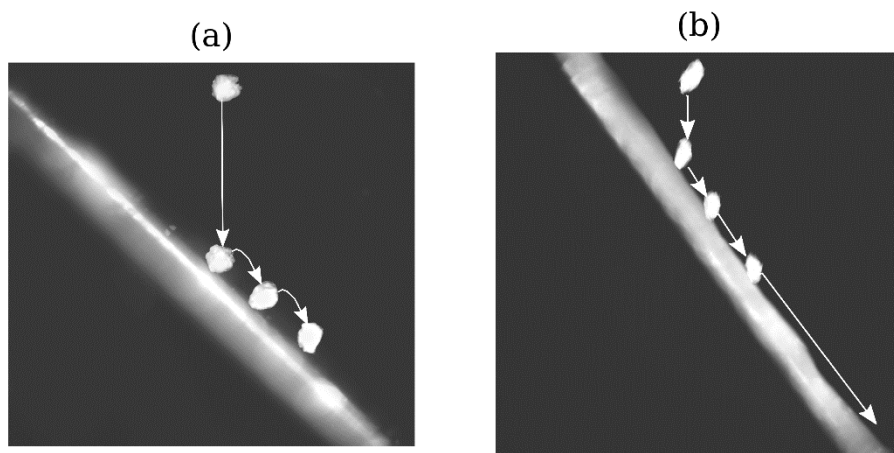
520

521 Figure 3. (a) Frequency spectrum for the plate response corresponding to a 100 μm particle
 522 collision. (b) Calculated frequencies corresponding to particles between 100 and 7150 μm particle
 523 collision with the plate at its epicenter. (c) Maximum amplitude and recorded frequency of
 524 particles between 100 and 7150 μm.



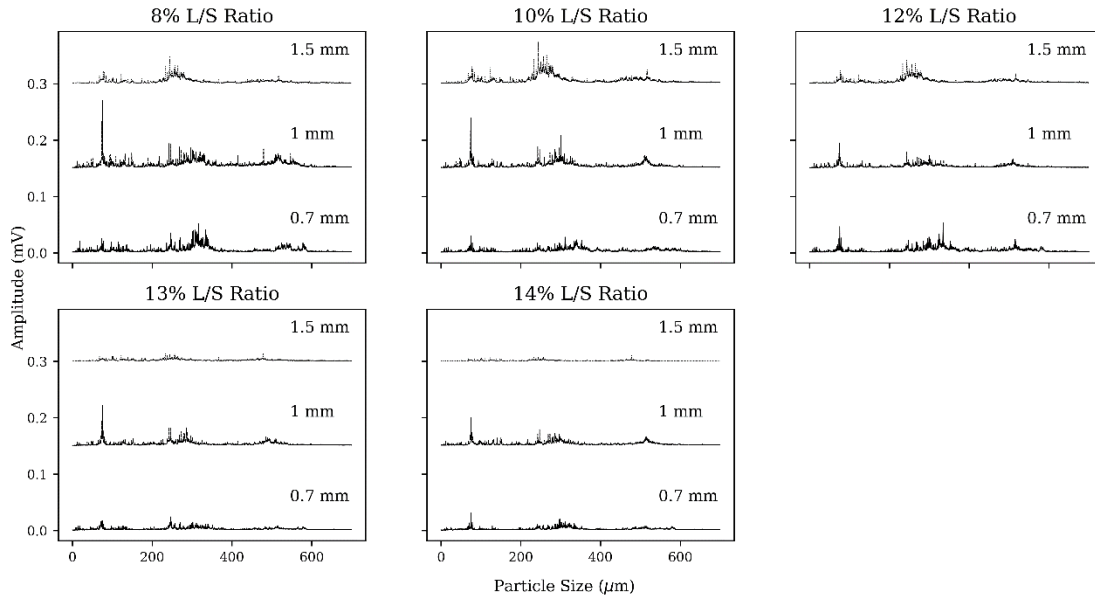
525

526 Figure 4. Average maximum amplitude of the AE spectra corresponding to changing incline plate
 527 angle.



528

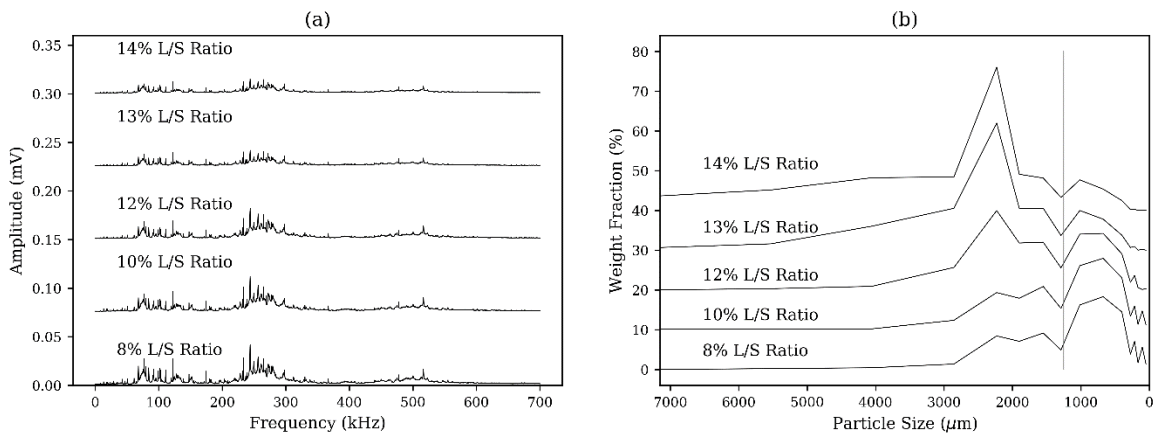
529 Figure 5. Trajectory of a particle on the impact plate with (a) 45 and (b) 60 degrees angle relative
 530 to the horizontal plate shown by super-imposing images over time. Arrows were shown to
 531 highlight the observed particle path followed.



532

533 Figure 6. AE spectra for each L/S ratio for the impact plate inclined at 60 degrees for thicknesses

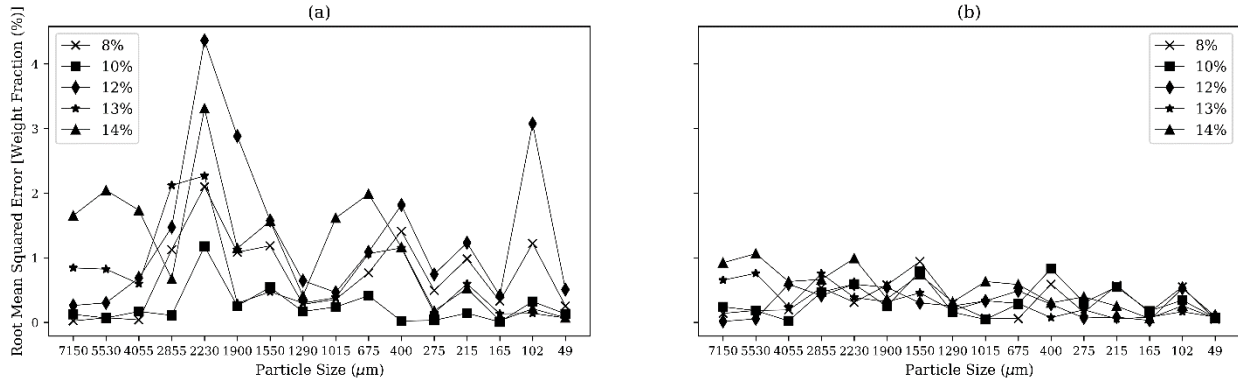
534 of 0.7, 1, and 1.5 mm.



535

536 Figure 7. (a) Acoustic spectra of particle impacts for each L/S ratio. (b) PSDs for each L/S ratio.

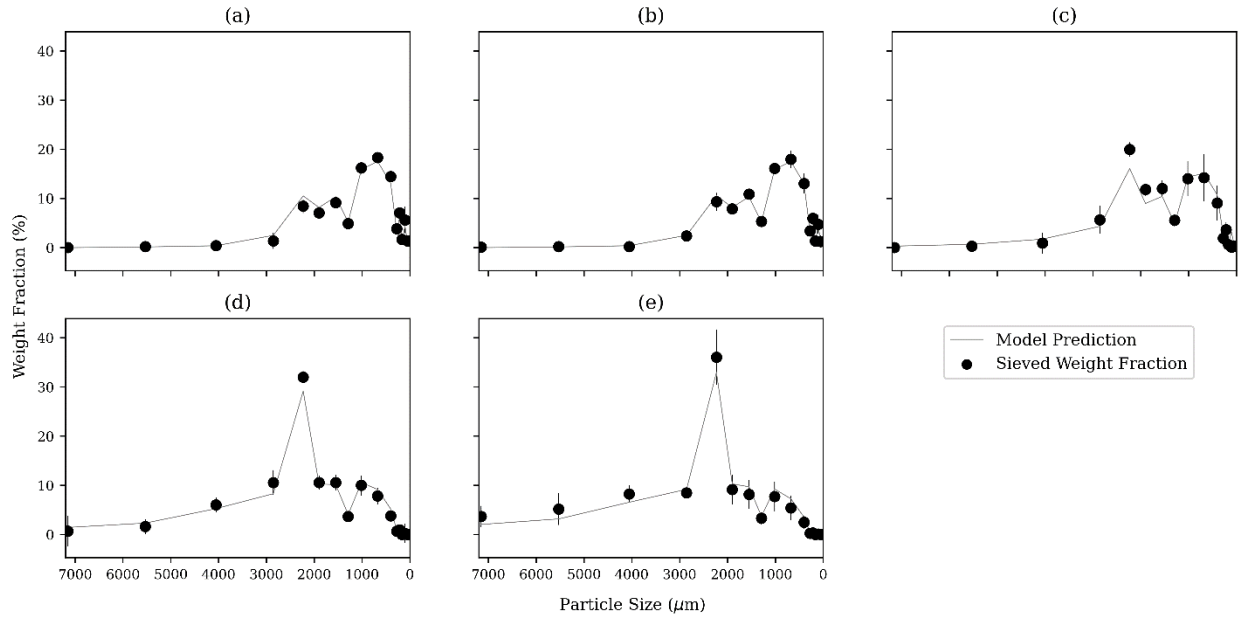
537 The vertical line indicates the often considered ideal size (1250 μm) suitable for tableting.



538

539 Figure 8. RMSE for every particle size at different L/S ratios for AE data (a) without and (b)

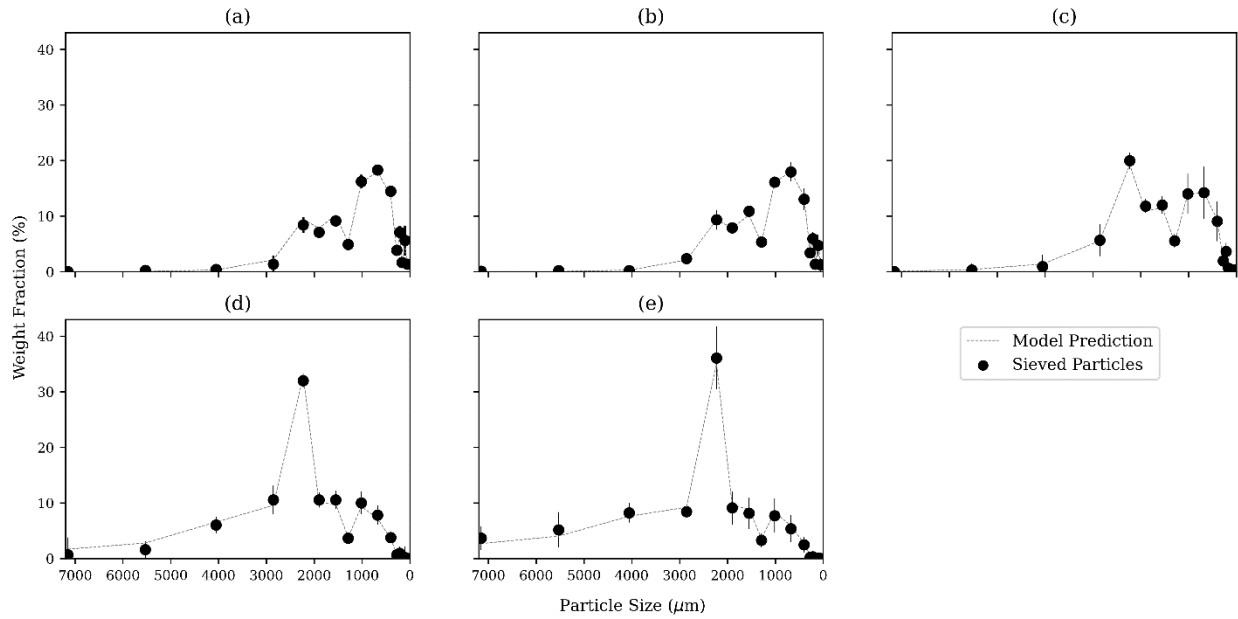
540 with the impact filter.



541

542 Figure 9. PSD predictions for (a) 8% (b) 10% (c) 12% (d) 13% and (e) 14% L/S ratio for AE

543 spectral data without the impact filter. Error bars represent the standard deviation (n=3).



544

545 Figure 10. PSD predictions for (a) 8% (b) 10% (c) 12% (d) 13% and (d) 14% L/S ratio for AE

546 spectral data with the impact filter. Error bars represent the standard deviation (n=3).

547